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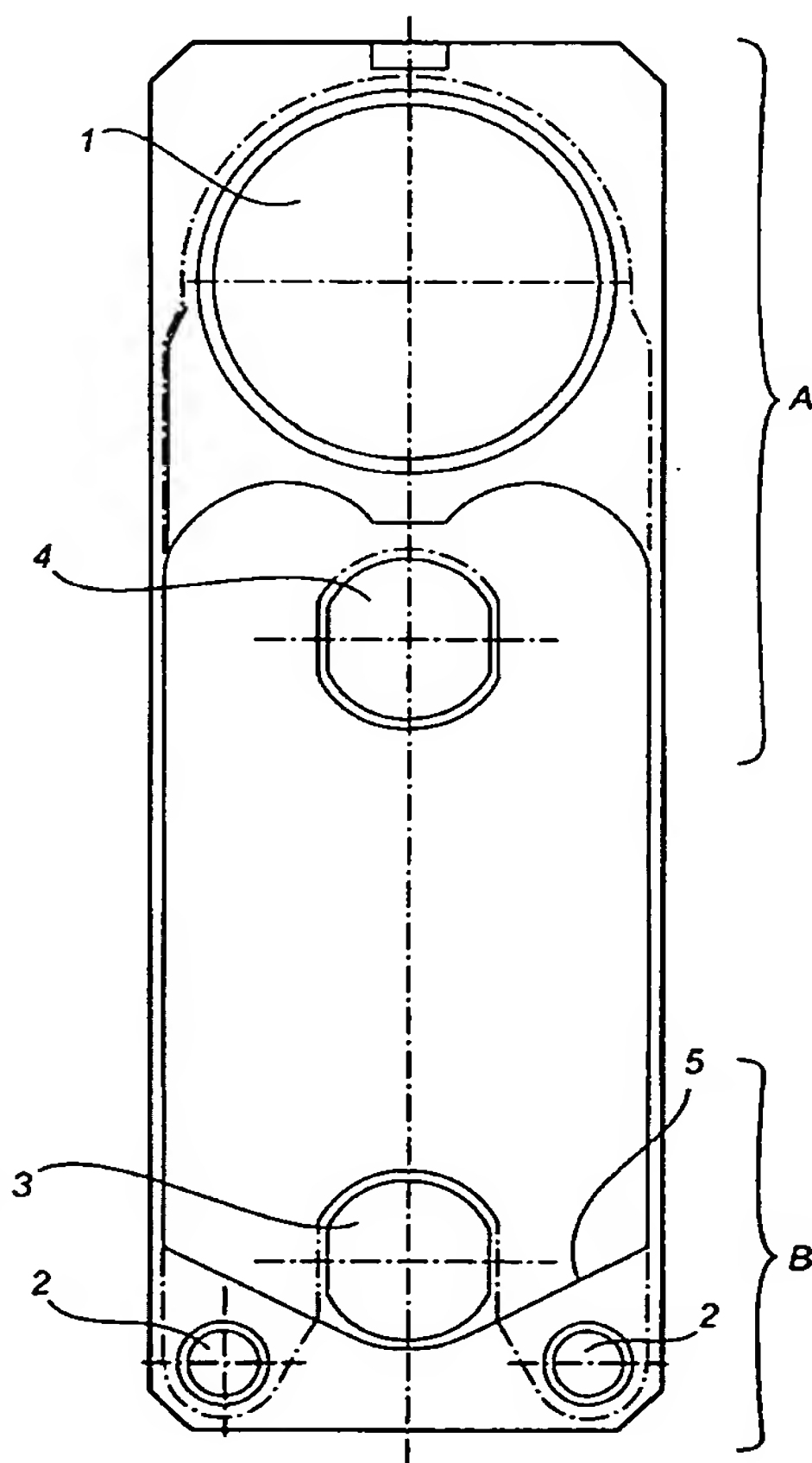
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(54) Title: **HEAT TRANSFER PLATE, PLATE PACK AND PLATE HEAT EXCHANGER**



(57) Abstract: A heat transfer plate for a plate heat exchanger comprises a first port portion (A), a second port portion (B), and a heat transfer portion, which is disposed between said port portions (A, B). The first port portion (A) comprises a first vapour inlet port (1) which is intended for a first fluid in vapour form and which extends over essentially the whole width of the plate. The second port portion (B) comprises at least one first outlet port (2), which is intended for condensed vapour. The first port portion (A) comprises a second outlet port (4), which is disposed between said vapour inlet port (1) and the second port portion (B) and which is intended for a second fluid. The second port portion (B) comprises a second inlet port (3), which is intended for said second fluid.

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HEAT TRANSFER PLATE, PLATE PACK AND PLATE HEAT EXCHANGERField of the Invention

The present invention relates to a heat transfer plate for a plate heat exchanger, comprising a first port portion which is disposed in one edge portion of the heat transfer plate, a second port portion which is disposed in a second edge portion of the heat transfer plate, and a heat transfer portion which is disposed between said port portions. The invention also relates to a plate pack and a plate heat exchanger.

10

Background Art

A plate heat exchanger comprises a plate pack consisting of a number of assembled heat transfer plates forming between them plate interspaces. Generally, every second plate interspace communicates with a first inlet channel and a first outlet channel, each plate interspace being adapted to define a flow area and to conduct a flow of a first fluid between said inlet and outlet channels. Correspondingly, the other plate interspaces communicate with a second inlet channel and a second outlet channel for a flow of a second fluid. Thus, the plates are in contact with one fluid through one of their side surfaces and with the other fluid through the other side surface, which allows a considerable heat exchange between the two fluids.

25

Modern plate heat exchangers have heat transfer plates, which in most cases are made of sheet-metal blanks that have been pressed and punched to obtain their final shape. Each heat transfer plate is usually provided with four or more "ports" consisting of through holes punched in the four corners of the plate. Sometimes, additional ports are punched along the short sides of the plates so as to be located between the ports punched in the corners. The ports of the different plates define

30

said inlet and outlet channels, which extend through the plate heat exchanger transversely of the plane of the plates. Gaskets or any other form of sealing means are arranged round some of the ports alternately in every
5 second plate interspace and, in the other plate interspaces, round the other ports so as to form the two separate channels for the first fluid and the second fluid, respectively.

Since considerable fluid pressure levels are obtained in the heat exchanger during operation, the plates
10 need to be sufficiently rigid so as not to be deformed by the fluid pressure. The use of plates made of sheet-metal blanks is possible only if the plates are somehow supported. Generally, this is achieved by the heat transfer
15 plates being provided with some kind of corrugation so that the plates bear against each other in a large number of points.

The plates are clamped together between two flexurally rigid end plates (or frame plates) in a "frame"
20 and thus form rigid units with flow channels in each plate interspace. The end plates are clamped together by means of a number of clamp bolts, which engage both plates by the intermediary of recesses or holes made along the circumference of each end plate.

25 In recent years, plate heat exchangers have come into use in applications in which at least one of the fluids is subjected to a phase change (condensation or evaporation). In many processes, vapour is used for heating purposes for two reasons: on the one hand vapour
30 contains a lot of energy that is released upon condensation and, on the other hand, the heating temperature is essentially constant. In the case of condensation temperatures exceeding 100°C the temperature cannot be regulated by means of, for instance, a so-called vapour
35 trap, which regulates the pressure of the condensate discharged. In the case of temperatures below 100°C vapour traps do not work for natural reasons - no

pressure can be achieved below atmospheric pressure. Instead, a condenser in which residual vapour is condensed must be used.

Conventional plate heat exchangers are not very well adapted for this task because of their symmetric design; ports of the same size and the same channel characteristic in both channels. In a typical application, the relationship between the vapour flow and the flow of cooling water is such that the diameter of the vapour inlet should be twice as large as that of the cooling water ports. Moreover, the channels in the plate inter-spaces should be highly asymmetric. The vapour requires a channel with a large cross-sectional area and low frictional resistance in order for the pressure drop to be minimized, and the cooling water requires a narrow channel with large frictional resistance that causes heavy turbulence.

In applications of this kind, the plates should have relatively large vapour ports to prevent the vapour phase pressure drop at the port or ports from becoming too great, which would have a detrimental effect on the efficiency of the heat exchanger. To allow for the provision of ports in a plate heat exchanger of the type mentioned above the plates have to be wide. This implies poor utilisation of the sheet-metal, which in turn makes the plate heat exchanger too expensive.

In this context, also the type of plate heat exchanger as described in DE-A1-19716200 should be mentioned. This publication discloses a plate heat exchanger in which all ports, i.e. also the ports for the different fluids, are positioned along one and the same line. The object stated in the DE publication is that it is desirable to obtain an improved distribution of the flow over the width of the heat transfer plates. The shape of the plate is essentially long and narrow and rectangular, and the two ports for one of the fluids are positioned at the

outer end of each short side of the plate whereas the two ports for the other fluid are positioned inside the same.

Furthermore, GB 2121525 discloses an evaporator or condenser made up of plates having respectively a long
5 and narrow upper port and a long and narrow lower port intended for a first fluid, which is to be conducted to every second plate interspace. The two ports extend over the whole width of the plate. The plate further comprises a number of protrusions which are disposed outside the
10 width of the plate and which each consist of a thin sheet-metal ring enclosing the corresponding port. These ports are intended to conduct a second fluid to the other plate interspaces. However, in this construction the frame plates must be of considerable size, since they
15 need to extend over the whole width of the plate as well as the protrusions.

Nor does the design disclosed in US 4,523,638 satisfy the design requirements stated above regarding efficient utilisation of the sheet-metal. Moreover, in
20 this US publication the ports are disposed in conventional manner, i.e. one port in each corner. The preamble to claim 1 is based on such a conventional condenser.

Finally, EP 411,123 discloses a special type of falling-film condenser in which the inlet port and the
25 outlet ports for the liquid are disposed adjacent to the lower edge. This particular type of condenser is intended for processes involving heat sensitive products, such as fruit juice, unrefined sugar solutions or the like, and does not provide any solution to the problems related
30 above.

Summary of the Invention

An object of the invention is to provide a solution to the problems stated above. A particular object of the
35 invention is to provide a design which allows improved utilisation of the material of the heat transfer plates. Furthermore, the design must be such that satisfactory

distribution of the fluid flow over the width of the plate is obtained. Further objects and advantages of the invention will be apparent from the following description.

5 The objects of the invention are achieved by means of a heat transfer plate, which is of the type stated above and which is characterised in that the first port portion comprises a first vapour inlet port which is intended for a first fluid in vapour form and which
10 extends over essentially the whole width of the plate, that the second port portion comprises at least one first outlet port which is intended for condensed vapour, that the first port portion comprises a second outlet port which is disposed between said vapour inlet port and the
15 second port portion and which is intended for a second fluid, and that the second port portion comprises a second inlet port which is intended for said second fluid. This port configuration is intended for use in applications in which the fluid undergoing a phase change
20 changes from vapour to condensate, i.e. the heat exchanger acts as a condenser.

 The invention may also be used for the opposite phase change, i.e. from liquid to vapour. In this case, the heat exchanger will act as an evaporator. The plate
25 will have essentially the same design in both cases. The objects stated above are achieved by means of the plate intended for a phase change from liquid to vapour, which plate is of the type mentioned above and which is characterised in that the first port portion comprises a first
30 vapour outlet port which is intended for a first fluid in vapour form and which extends over essentially the whole width of the plate, that the second port portion comprises at least one first inlet port which is intended for said first fluid in liquid form, that the first port
35 portion comprises a second inlet port which is disposed between said vapour outlet port and the second port portion and which is intended for a second fluid, and

that the second port portion comprises a second outlet port which is intended for said second fluid.

By designing the heat transfer plate in this manner, an extremely advantageous utilisation of the sheet-metal is obtained as well as a very high degree of efficiency of the condenser or evaporator. The large vapour port extending over essentially the whole width of the plate provides a vapour flow in which essentially no drop in pressure occurs. By arranging the port for the second fluid in the first port portion between the vapour port and the second port portion, benefit may be derived from the fact that, in connection with the phase change, only a relatively short distance is required in the direction of flow where the heat exchange takes place. By arranging the ports in two opposite port portions, the intermediate plate area is optimally utilised to achieve the desired heat exchange.

Preferred embodiments of the invention are apparent from the dependent claims.

According to a preferred embodiment, said second inlet port and said second outlet port have essentially the same port area. Since no phase change takes place in the fluid, which passes through these ports, the rate of flow is the same through the two ports. This embodiment affords the lowest pressure drop and, thus, is the most efficient.

Advantageously, said second inlet port has a port area of about 10-50%, preferably 15-40% and most preferred 20-30%, of the corresponding port area of said vapour inlet or vapour outlet port. This affords a particularly good relationship between the vapour supplied or discharged in the form of vapour and the fluid supplied or discharged in the form of liquid, which results in a high degree of efficiency of the plate heat exchanger. Moreover, owing to the large vapour port the vapour flow will not be subjected to any appreciable pressure drop.

According to a preferred embodiment, said at least one first outlet port intended for condensed vapour or first inlet port intended for the first fluid in liquid form comprises two ports, which are disposed in two
5 corners of the heat transfer plate. In this manner, use can be made of the small corners of the plate, which would otherwise not have been used. During the phase change into liquid, the vapour releases a large amount of heat per weight unit to the second fluid, which means
10 that it is possible to use a rate of flow which when measured in the condensed state is relatively small. This allows the use of relatively small ports, which may be arranged in such manner that the best possible use is made of the metal-sheet surface.

15 In a preferred embodiment, the port disposed in the second port portion and intended for the second fluid is arranged between said at least one port intended for the first fluid and the first port portion. This means that satisfactory flow distribution of the condensed vapour or
20 of the liquid to be evaporated is obtained over the whole width of the plate, since the port intended for the second fluid will by itself force the flow stream to be distributed as it flows adjacent to the port.

According to another preferred embodiment, the ports
25 in the second port portion, which are intended for said first fluid and said second fluid, are disposed next to each other at essentially the same distance from the first port portion. This design implies an advantageous use of the plate surface.

30 According to yet another preferred embodiment, the port disposed in the first port portion and intended for the second fluid is offset relative to the vapour inlet or vapour outlet port in such manner that it is located along an edge of the plate. It is thus possible to ensure
35 that a minimum pressure drop is obtained for the vapour port formed in the first port portion, which in turn

makes it possible to obtain a higher degree of efficiency in the plate heat exchanger.

According to a preferred embodiment, the plate is symmetric about its longitudinal axis. This is preferred
5 from the point of view of manufacture since it allows one single plate type to be used alternately by rotating every second plate a half turn about its symmetry axis.

The above objects are also achieved by means of a plate pack comprising a plurality of heat transfer plates
10 of the types mentioned above.

In the plate pack, said first inlet port of the heat transfer plates forms a first inlet channel through the plate pack, said first outlet port forms a first outlet channel through the plate pack, said second inlet port of
15 the heat transfer plates forms a second inlet channel through the plate pack and said second outlet port of the heat transfer plates forms a second outlet channel through the plate pack, the first inlet channel and the first outlet channel being in fluid communication with
20 each other via a first set of plate interspaces and the second inlet channel and the second outlet channel communicating with each other via a second set of plate interspaces.

Advantageously, each of the plate interspaces in the
25 first set has a channel height or volume that is greater than each of the plate interspaces in the second set. This allows a high degree of efficiency to be obtained. The vapour pressure drop will be small and a large amount of vapour can be supplied, which is desirable since the
30 vapour has a considerably larger volume than a liquid. Moreover, the second fluid will be subjected to a greater pressure drop, the second fluid flow will be more turbulent and the heat transfer more efficient.

The objects stated above are also achieved by means
35 of a plate heat exchanger comprising a number of heat transfer plates of the type stated above and by means of

a plate heat exchanger comprising a number of plate packs of the type stated above.

Brief Description of the Drawings

5 The invention will be described in more detail below with reference to the accompanying schematic drawings, which by way of example illustrate currently preferred embodiments of the invention.

10 Fig. 1 shows a heat transfer plate according to a first embodiment of the invention.

 Fig. 2 shows a heat transfer plate according to a second embodiment of the invention.

Detailed Description of Preferred Embodiments

15 As shown in Figs 1 and 2, the heat transfer plate according to the preferred embodiments has a long and narrow, essentially rectangular shape. A port portion A, B is provided on both short sides. In the respective port portions through holes, called ports 1-4, are provided.
20 These heat transfer plates are adapted to be assembled into a plate pack in conventional manner, so that each of the ports forms a channel extending through the plate pack of the plate heat exchanger (not shown).

 For the sake of simplicity, the heat transfer plates
25 described below will be adapted for use in applications in which the fluid undergoing a phase change changes from vapour to condensate. In other words, the heat transfer plates described will be adapted for use in a condenser. For the opposite phase change, i.e. from liquid to vapour
30 (evaporator), the heat transfer plates will have essentially the same design.

 The first port 1 forms a first inlet channel, which is intended for a first fluid, whereas the second port 2 forms a first outlet channel, which is intended for said
35 fluid. The third port 3 forms a second inlet channel, which is intended for a second fluid and the fourth port 4 forms a second outlet channel, which is intended for

said fluid. Generally, every second plate interspace communicates with the first inlet channel and the first outlet channel, each plate interspace being adapted to define a flow area and to conduct a flow of the first fluid between said inlet and outlet channels. Correspondingly, the other plate interspaces communicate with the second inlet and outlet channel for a flow of the second fluid. Thus, the plates are in contact with one fluid through one of their side surfaces and with the other fluid through the other side surface, which allows a considerable heat exchange between the two fluids.

In Figs 1 and 2, sealing gaskets 5 which extend round the second inlet port 3 and the second outlet port 4 are indicated by unbroken lines. A similar gasket is provided on every second heat transfer plate of the plate pack. On the intermediate heat transfer plates, a gasket is provided which extends round the first inlet port 1 and the first outlet port 2. These gaskets contribute to the formation of separate channels through the plate heat exchanger, one for the first heat exchanging fluid and one for the second heat exchanging fluid.

The above description, in which specific embodiments have not been taken into particular consideration, is applicable to the embodiments described below unless otherwise stated in connection with the description of the respective embodiments.

In the embodiment shown in Fig. 1, the heat transfer plate comprises a first vapour inlet port 1 in the upper port portion A. The vapour inlet port 1 is intended for a first fluid in vapour form and extends over essentially the whole width of the heat transfer plate. Furthermore, the port portion A comprises a second outlet port 4, which is disposed along the same geometric centre line as the vapour inlet port 1 and arranged between the first vapour inlet port 1 and the lower port portion B.

The lower port portion B comprises a second inlet port 3, which is disposed along said geometric centre

line. As shown in Fig. 1, said second inlet port 3 and said second outlet port 4 have essentially the same port area. The ports 3, 4 have a port area of about 10-50%, preferably 15-40% and most preferred 20-30%, of the
5 corresponding port area of the vapour inlet port 1.

The lower port portion B further comprises two first outlet ports 2, which are disposed in the two corners of the heat transfer plate. The outlet ports 2 form outlet channels for a condensate through the plate pack.

10 Fig. 2 illustrates a second embodiment of the heat transfer plate shown in Fig. 1. As shown in Fig. 1, the heat transfer plate comprises a vapour inlet port 1, which is disposed in the upper port portion A. The port portion A further comprises a second outlet port 4, which
15 in this second embodiment is offset relative to said vapour inlet port 1. The second outlet port 4 is disposed along one side portion of the heat transfer plate.

The lower port portion B comprises a first outlet port 2 and a second inlet port 3. Said outlet and inlet
20 ports 2, 3 are disposed next to each other in the two corners of the heat transfer plate.

The second inlet port 3 and the second outlet port 4 have essentially the same port area also in this second embodiment. The size of said ports corresponds to the
25 size described in the first embodiment.

It will be appreciated that various modifications of the embodiments of the invention described above are possible within the scope of the invention, as defined by the appended claims. For example, the position of the
30 ports on the heat transfer plate and their relative sizes may be slightly adjusted in different applications.

CLAIMS

1. A heat transfer plate for a plate heat exchanger,
5 preferably a condenser, comprising
a first port portion (A) which is disposed in one
edge portion of the heat transfer plate,
a second port portion (B) which is disposed in a
second edge portion of the heat transfer plate, and
10 a heat transfer portion which is disposed between
said port portions (A, B), c h a r a c t e r i s e d in
that the first port portion (A) comprises a first
vapour inlet port (1) which is intended for a first fluid
in vapour form and which extends over essentially the
15 whole width of the plate,
that the second port portion (B) comprises at least
one first outlet port (2) which is intended for condensed
vapour,
that the first port portion (A) comprises a second
20 outlet port (4) which is disposed between said vapour
inlet port (1) and the second port portion (B) and which
is intended for a second fluid, and
that the second port portion (B) comprises a second
inlet port (3) which is intended for said second fluid.
25 2. A heat transfer plate for a plate heat exchanger,
preferably an evaporator, comprising
a first port portion (A) which is disposed in one
edge portion of the heat transfer plate,
a second port portion (B) which is disposed in a
30 second edge portion of the heat transfer plate, and
a heat transfer portion which is disposed between
said port portions (A, B), c h a r a c t e r i s e d in
that the first port portion (A) comprises a first
vapour outlet port (1) which is intended for a first
35 fluid in vapour form and which extends over essentially
the whole width of the plate,

that the second port portion (B) comprises at least one first inlet port (2) which is intended for said first fluid in liquid form,

that the first port portion (A) comprises a second
5 inlet port (4) which is disposed between said vapour outlet port (1) and the second port portion (B) and which is intended for a second fluid, and

that the second port portion (B) comprises a second outlet port (3) which is intended for said second fluid.

10 3. A heat transfer plate according to claim 1 or 2, wherein the port (3) and the port (4) have essentially the same port area.

4. A heat transfer plate according to any one of the preceding claims, wherein the port (3) has a port area
15 that is 10-50%, preferably 15-40% and most preferred 20-30%, of the corresponding port area of said vapour inlet or said vapour outlet port (1).

5. A heat transfer plate according to any one of the preceding claims, wherein said at least one first outlet
20 port intended for condensed vapour or first inlet port (2) intended for a first fluid in liquid form comprises two ports which are disposed in two corners of the heat transfer plate.

6. A heat transfer plate according to any one of the
25 preceding claims, wherein the port (3) which is disposed in the second port portion (B) and intended for the second fluid is arranged between said at least one port intended for the first fluid and the first port portion.

7. A heat transfer plate according to any one of
30 claims 1-5, wherein the ports (2, 3) in the second port portion (B), which are intended for said first fluid and said second fluid, are disposed next to each other at essentially the same distance from the first port portion (A).

35 8. A heat transfer plate according to any one of the preceding claims, wherein the port which is disposed in the first port portion (A) and intended for the second

fluid is offset relative to the vapour inlet or vapour outlet port (1) in such manner that it is located along an edge of the plate.

9. A heat transfer plate according to any one of
5 claims 1-7, which is symmetric about its longitudinal axis.

10. A plate pack for a plate heat exchanger,
c h a r a c t e r i s e d in that it comprises a plu-
rality of heat transfer plates of the type stated in any
10 one of claims 1-9.

11. A plate pack according to claim 10, wherein said
first inlet port of the heat transfer plates forms a
first inlet channel through the plate pack, said first
outlet port (2) forms a first outlet channel through the
15 plate pack, said second inlet port (3) of the heat trans-
fer plates forms a second inlet channel through the plate
pack and said second outlet port (4) of the heat transfer
plates forms a second outlet channel through the plate
pack, the first inlet channel and the first outlet chan-
20 nel being in fluid communication with each other via a
first set of plate interspaces and the second inlet chan-
nel and the second outlet channel communicating with each
other via a second set of plate interspaces, and each of
the plate interspaces in the first set having a channel
25 height that is greater than each of the plate interspaces
in the second set.

12. A plate heat exchanger, c h a r a c t e r -
i s e d in that it comprises a number of heat transfer
plates of the type stated in any one of claims 1-9.

30 13. A plate heat exchanger, c h a r a c t e r -
i s e d in that it comprises a number of plate packs of
the type stated in claim 10.

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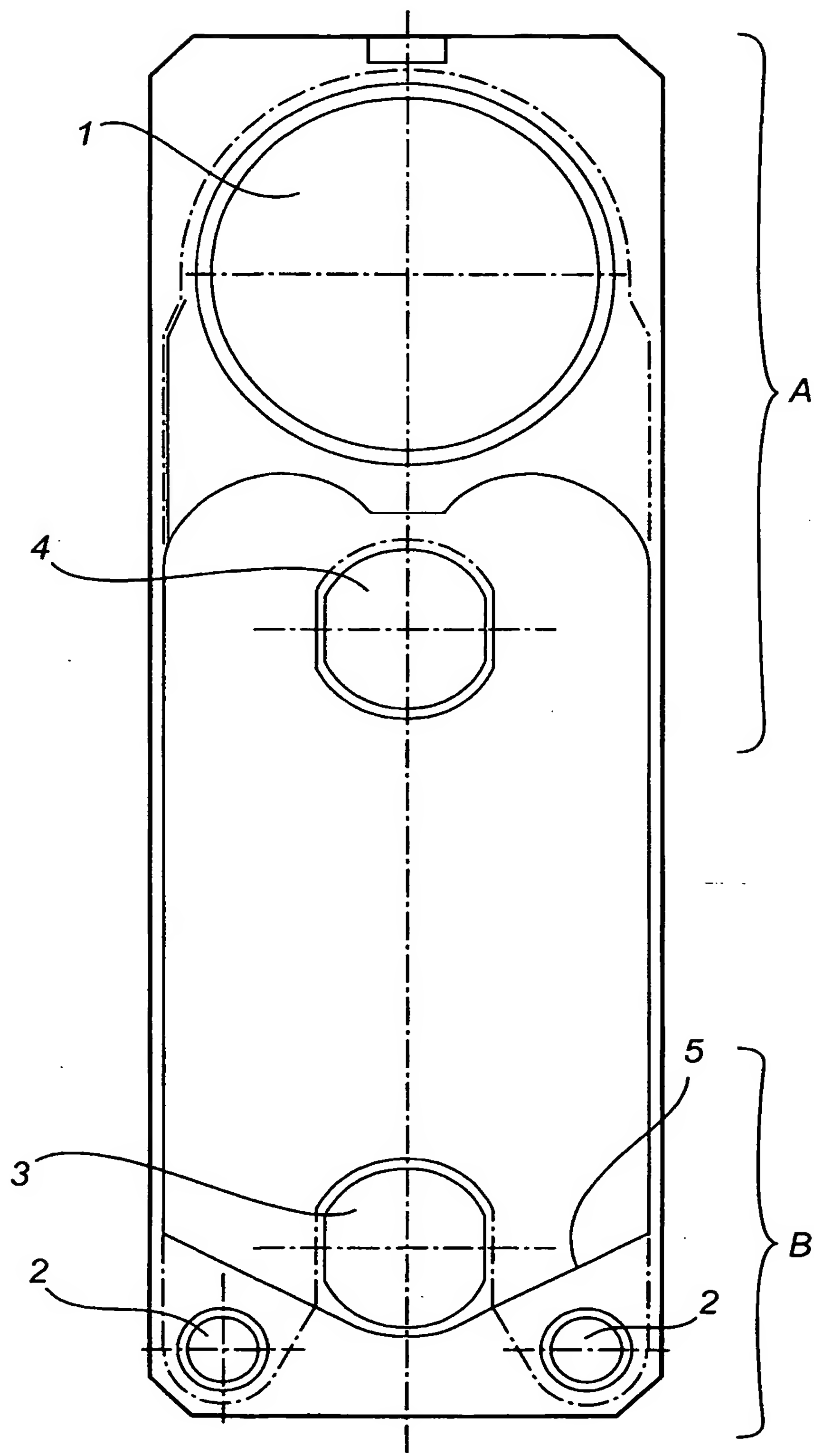


Fig. 1

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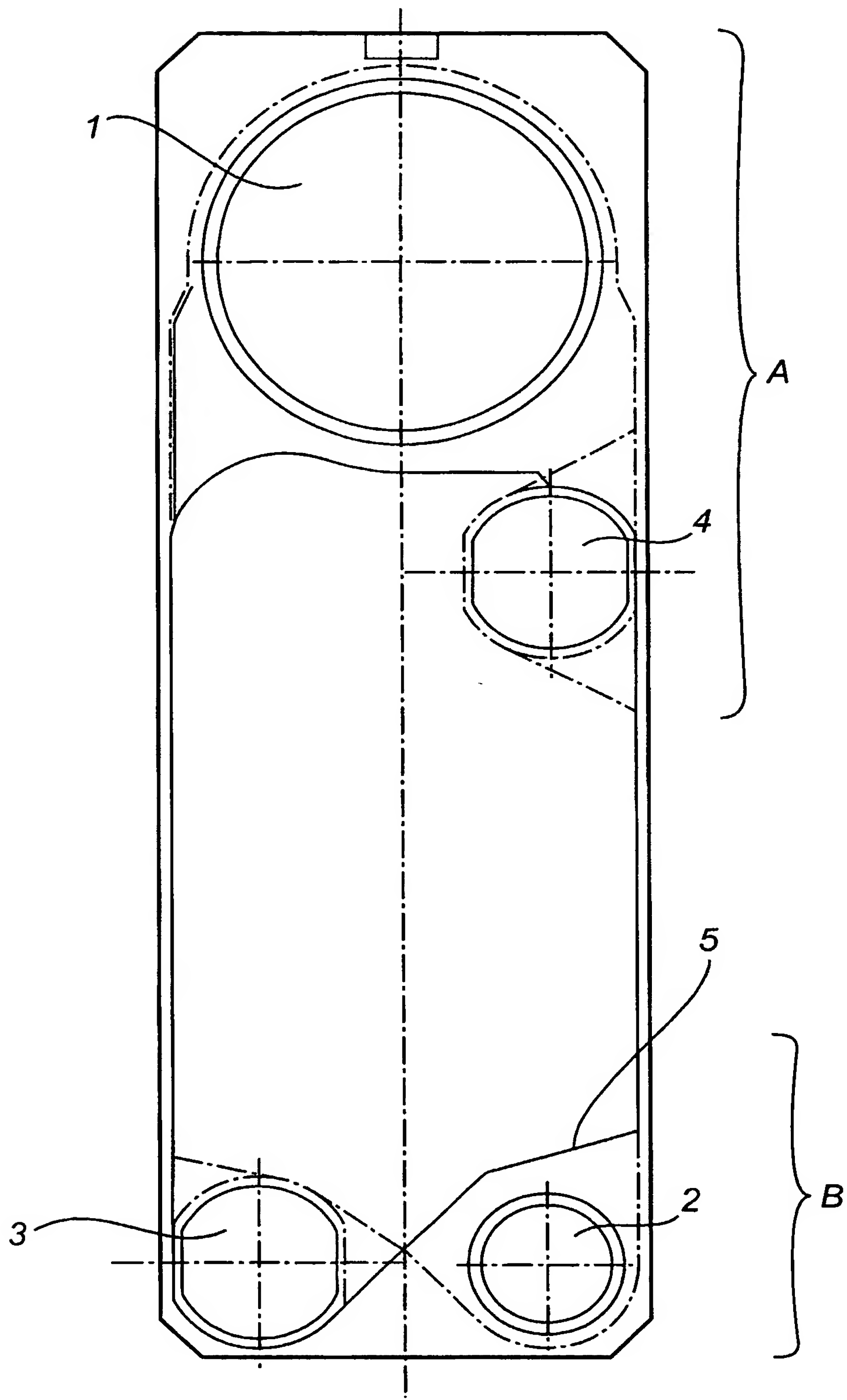


Fig. 2

INTERNATIONAL SEARCH REPORT

International application No.

PCT/SE 02/01063

A. CLASSIFICATION OF SUBJECT MATTER

IPC7: F28F 3/08, F28D 9/00

According to International Patent Classification (IPC) or to both national classification and IPC

B. FIELDS SEARCHED

Minimum documentation searched (classification system followed by classification symbols)

IPC7: F28D, F28F

Documentation searched other than minimum documentation to the extent that such documents are included in the fields searched

SE,DK,FI,NO classes as above

Electronic data base consulted during the international search (name of data base and, where practicable, search terms used)

EPO-INTERNAL, WPI DATA, PAJ

C. DOCUMENTS CONSIDERED TO BE RELEVANT

Category*	Citation of document, with indication, where appropriate, of the relevant passages	Relevant to claim No.
X	US 4523638 A (ROSMAN ET AL), 18 June 1985 (18.06.85) --	1-5,7-10,12, 13
A	DE 197162000 A1 (FUNKE WÄRMEAUSTAUSCHER APPARATEBAU GMBH), 22 October 1998 (22.10.98) --	
A	GB 2121525 A (W. SCHMIDT GMBH AND CO. KG), 21 December 1983 (21.12.83) --	
A	EP 0411123 A1 (HISAKA WORKS, LTD.), 6 February 1991 (06.02.91) --	

☒ Further documents are listed in the continuation of Box C.☒ See patent family annex.

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Date of the actual completion of the international search

26 August 2002

Date of mailing of the international search report

10-09-2002

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INTERNATIONAL SEARCH REPORT

International application No. PCT/SE 02/01063
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C (Continuation). DOCUMENTS CONSIDERED TO BE RELEVANT		
Category*	Citation of document, with indication, where appropriate, of the relevant passages	Relevant to claim No.
A	SE 514682 C2 (SWEP INTERNATIONAL AB), 2 April 2001 (02.04.01) -----	

INTERNATIONAL SEARCH REPORT

Information on patent family members

06/07/02

International application No.

PCT/SE 02/01063

Patent document cited in search report			Publication date	Patent family member(s)	Publication date
US	4523638	A	18/06/85	US 4347896 A	07/09/82
				US 4503908 A	12/03/85
				US 4535840 A	20/08/85
				US 4749032 A	07/06/88
DE	197162000	A1	22/10/98	NONE	
GB	2121525	A	21/12/83	AT 151783 A	15/09/88
				AT 387914 B	10/04/89
				BR 8302831 A	17/01/84
				DE 3220774 A,C	08/12/83
				FR 2528164 A,B	09/12/83
				GB 8313394 D	00/00/00
				IT 1167417 B	13/05/87
				IT 8348347 D	00/00/00
				JP 1357149 C	13/01/87
				JP 58223401 A	26/12/83
				JP 61021681 B	28/05/86
				SE 463016 B,C	01/10/90
				SE 8303090 A	03/12/83
				US 4572766 A	25/02/86
EP	0411123	A1	06/02/91	SE 0411123 T3	
				BR 8907347 A	30/04/91
				DE 68922308 D,T	09/11/95
				US 5098518 A	24/03/92
				WO 9009220 A	23/08/90
SE	514682	C2	02/04/01	EP 1173916 A	23/01/02
				SE 0000591 A	02/04/01
				WO 0163174 A	30/08/01

11/11/11

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